

CONCENTRATION OF BIOPETROL SYNTHESIZED FROM OLEIC ACID
THROUGH HETEROGENEOUS CATALYTIC CRACKING USING ZEOLITE AS
CATALYST

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ABSTRACT

One of the main fatty acids in vegetable oil is oleic acid and it has the potential to replace petroleum fuels in the future. In this research, zeolite catalysts are used over the conversion of oleic acid into isooctane as the future biopetrol in a heating mantle at atmospheric pressure. The main purposed of studies is to improve the concentration of isooctane using heterogeneous catalytic cracking method with using 20g of zeolite catalysts. The effect of various rotation speed of sample at 600 rpm, 780 rpm, 960 rpm and 1140 rpm and dilution factor of isooctane to hexane at 10% are studied over the yield of biopetrol at 98°C. Gas chromatography is used for the qualitative and quantitative analysis of the samples. Backward calculation is applied to calculate the actual concentration of isooctane in the distilled oleic acid. The maximum yield of desired isooctane obtained at 1140 rpm with 20g of catalyst and dilution of 10% isooctane to hexane is recorded at 11.67 %. Experimental works has successful show that heterogeneous catalytic cracking is greater in conversion than catalytic cracking (static catalyst) and thermal cracking.

ABSTRAK

Salah satu asid lemak utama di dalam minyak sayuran ialah asid oleic dan ianya mempunyai potensi yang tinggi untuk menggantikan bahan api petroleum dimasa depan. Dalam kajian ini, agen pemangkin Zeolite telah digunakan untuk memperolehi isooktana daripada asid oleik untuk dijadikan sebagai biopetrol pada masa akan datang dengan menggunakan pemanas mantel pada tekanan atmosfera. Tujuan utama kajian ini dijalankan adalah untuk memperbaiki kepekatan isooktana menggunakan kaedah penguraian agen pemangkin. Kesan perubahan jumlah kelajuan pusingan sampel pada kelajuan 600 ppm, 780 ppm, 960 ppm dan 1140 ppm serta faktor pencairan isooktana kepada heksana pada 10% dikaji terhadap penghasilan biopetrol pada suhu 98°C. Alat Gas Kromatografi telah digunakan untuk kualitatif dan kuantitatif analisis semua sampel. Pengiraan semula kepekatan isooktana tanpa pencairan heksana digunakan untuk mengira kepekatan sebenar isooktana di dalam didihan asid oleik. Kepekatan maksimum isooktana dicatatkan pada 1140 ppm dengan 20g agen pemangkin dan pada 10% cairan isooktana kepada heksana iaitu sebanyak 11.67%. Experimen ini telah berjaya membuktikan penguraian menggunakan kaedah agen pemangkin lebih bagus berbanding kaedah penguraian agen pemangkin (statik agen pemangkin) dan penguraian haba.

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LIST OF SYMBOLS

P	-	Pressure
m	-	Mass
ΔH	-	Enthalpy change of reaction
ΔS	-	Entropy change of reaction
ΔG	-	Energy change of reaction
T	-	Temperature
ρ	-	Density
μ	-	Viscosity of liquid (Pa.s)
h	-	Heat transfer coefficient
$^{\circ}\text{C}$	-	Degree Celsius
kg	-	Kilogram
K	-	Degree Kelvin
m	-	Meter
n	-	Number of moles
L	-	Liter
rpm	-	Rotation per minute
ppm	-	Pusingan per minit

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APPENDIX D

RESULT OF ISOOCTANE SAMPLES CHROMATOGRAM

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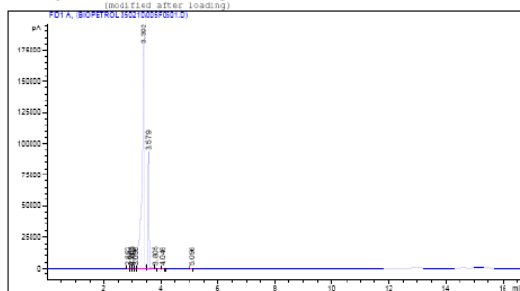


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Data File C:\CHEM32\1\DATA\BIOPETROL 05010\000F0031.D
Sample Name: 6.1

Acq. Operator : F12a080210 Seq. Line : 5
Acq. Instrument : Instrument 1 Location : Vial 5
Injection Date : 08/02/2010 13:01:48 Inj : 1
Inj Volume : 1 µl
Acq. Method : C:\CHEM32\1\METHODS\ISOCTANE230108.M
Last changed : 08/02/2010 11:27:14 by F12a080210
Analysis Method : C:\CHEM32\1\METHODS\FATINAH.M
Last changed : 23/03/2010 14:27:59 by f12a230310
(modified after loading)



Area Percent Report

Sorted By : Signal
Multiplier : 1.0000
Dilution : 1.0000
Use Multiplier & Dilution Factor with ISTDs

Signal 1: FID1 A,

Peak #	RetTime [min]	Type	Width [min]	Area [pA*s]	Height [pA]	Area %
1	2.852	BV	0.8320	48.34252	23.41971	0.00336
2	2.953	VV	0.8297	775.00403	397.33249	0.05382
3	3.003	VV	0.8366	1734.53855	719.46246	0.12045
4	3.098	VV	0.8432	176.34491	61.44441	0.01183
5	3.292	VV	0.1054	1.179605	1.8657465	91.91368
6	3.776	VB	0.8460	2.6476548	0.313564	3.83011
7	3.805	BB	0.8284	871.74005	485.49095	0.06054
8	4.046	BB	0.8287	58.56289	31.14177	0.00407
9	5.096	BV	0.8370	30.53894	11.67797	0.00212
Totals :				1.44006e6	2.81476e5	

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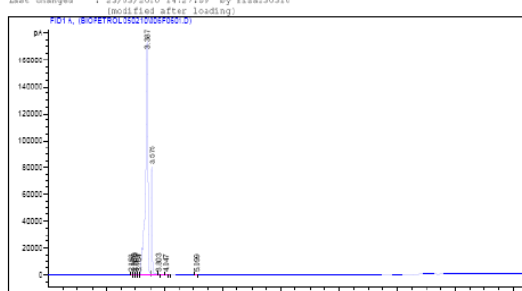
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Sample X1

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Sample Name: 6.2

Acq. Operator : F12a080210 Seq. Line : 6
Acq. Instrument : Instrument 1 Location : Vial 6
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Inj Volume : 1 µl
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Analysis Method : C:\CHEM32\1\METHODS\FATINAH.M
Last changed : 23/03/2010 14:27:59 by f12a230310
(modified after loading)



Area Percent Report

Sorted By : Signal
Multiplier : 1.0000
Dilution : 1.0000
Use Multiplier & Dilution Factor with ISTDs

Signal 1: FID1 A,

Peak #	RetTime [min]	Type	Width [min]	Area [pA*s]	Height [pA]	Area %
1	2.498	BB	0.3917	18.28450	8.40093	0.00155
2	2.959	BV	0.8301	491.12982	253.57837	0.44175
3	3.009	VV	0.8354	1204.49165	512.23737	0.10240
4	3.108	VV	0.8407	128.16335	48.15306	0.11089
5	3.287	VV	0.8921	9.6151665	1.7336065	95.72773
6	3.575	VB	0.8438	1.1204645	0.0615544	4.12531
7	3.803	BB	0.8293	722.15262	386.30143	0.06143
8	4.047	BB	0.8291	315.70944	166.53766	0.02683
9	5.099	BV	0.8393	24.44240	8.88871	0.00209
Totals :				1.17649e6	2.55550e5	

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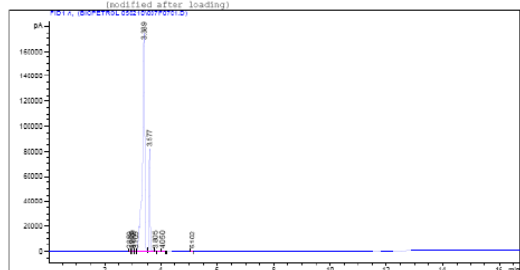
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Sample X2

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Sample Name: 6.3

Acq. Operator : F12a080210 Seq. Line : 7
Acq. Instrument : Instrument 1 Location : Vial 7
Injection Date : 08/02/2010 13:48:08 Inj : 1
Inj Volume : 1 µl
Acq. Method : C:\CHEM32\1\METHODS\ISOCTANE230108.M
Last changed : 08/02/2010 11:27:14 by F12a080210
Analysis Method : C:\CHEM32\1\METHODS\FATINAH.M
Last changed : 23/03/2010 14:27:59 by f12a230310
(modified after loading)



Area Percent Report

Sorted By : Signal
Multiplier : 1.0000
Dilution : 1.0000
Use Multiplier & Dilution Factor with ISTDs

Signal 1: FID1 A,

Peak #	RetTime [min]	Type	Width [min]	Area [pA*s]	Height [pA]	Area %
1	2.855	BB	0.8321	20.17507	9.58378	0.00189
2	2.955	BV	0.8302	494.13562	253.45474	0.04140
3	3.016	VV	0.8350	1198.41642	503.32039	0.10011
4	3.105	VV	0.8413	125.26886	48.10557	0.01063
5	3.281	VV	0.8981	9.7888648	1.7677648	91.77187
6	3.577	VB	0.8436	2.1432765	0.1844664	3.95782
7	3.805	BB	0.8291	737.02784	389.29092	0.06175
8	4.050	BB	0.8331	626.57056	316.77924	0.05250
9	5.101	BV	0.8394	22.91750	8.13618	0.00192
Totals :				1.19350e6	2.58153e5	

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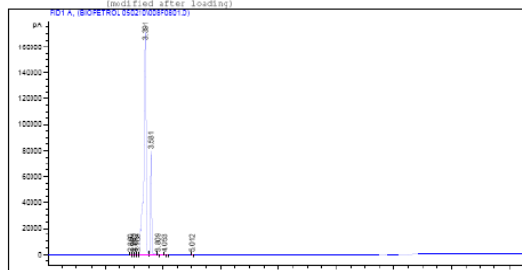
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Page 1 of 1

Sample X3

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Sample Name: 6.4

Acq. Operator : F12a080210 Seq. Line : 8
Acq. Instrument : Instrument 1 Location : Vial 8
Injection Date : 08/02/2010 14:11:11 Inj : 1
Inj Volume : 1 µl
Acq. Method : C:\CHEM32\1\METHODS\ISOCTANE230108.M
Last changed : 08/02/2010 11:27:14 by F12a080210
Analysis Method : C:\CHEM32\1\METHODS\FATINAH.M
Last changed : 23/03/2010 14:27:59 by f12a230310
(modified after loading)



Area Percent Report

Sorted By : Signal
Multiplier : 1.0000
Dilution : 1.0000
Use Multiplier & Dilution Factor with ISTDs

Signal 1: FID1 A,

Peak #	RetTime [min]	Type	Width [min]	Area [pA*s]	Height [pA]	Area %
1	2.860	BB	0.8311	22.74082	10.98553	0.00198
2	2.961	BV	0.8294	509.14935	264.82245	0.04432
3	3.012	VV	0.8358	1203.96277	515.33555	0.10480
4	3.108	VV	0.8402	125.26921	48.27297	0.01093
5	3.291	VV	0.8914	9.3958165	1.704145	91.78502
6	3.581	VB	0.8432	2.0600765	0.283284	3.86921
7	3.809	BB	0.8289	726.14099	391.91760	0.06321
8	4.053	BB	0.8299	62.41838	31.44631	0.00543
9	5.012	BV	0.8350	4.67523	2.09768	0.00041
Totals :				1.14884e6	2.51852e5	

*** End of Report ***

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Page 1 of 1

Sample X4

Figure D.2: Sample X

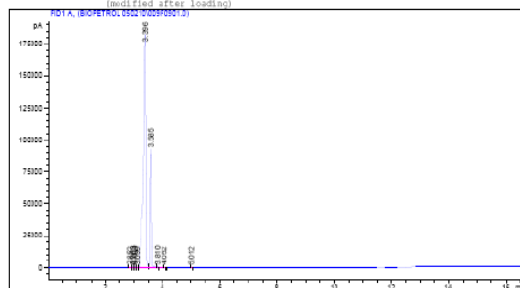
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Sample Name: 7.1

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Acq. Operator   : F11a080210                      Seq. Line : 9
Acq. Instrument : Instrument 1                      Location : Vial 9
Injection Date  : 08/02/2010 14:34:28              Inj : 1
                                                    Inj Volume : 1 µl
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Last changed   : 08/02/2010 11:27:14 by F11a080210
Analysis Method : C:\CHEM32\1\METHODS\FAT1PM9.M
Last changed   : 23/03/2010 14:27:59 by f11a230310
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Area Percent Report

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Dilution       : 1.0000
Use Multiplier & Dilution Factor with ISTDs
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Signal 1: FID1 A,

Peak #	RetTime [min]	Type	Width [min]	Area [pA*s]	Height [pA]	Area %
1	2.852	BB	0.0325	36.44353	16.84476	0.00255
2	2.853	VV	0.0305	682.24931	346.23414	0.04766
3	3.004	VV	0.0372	1543.14909	633.4222	0.10920
4	3.099	VV	0.0436	166.46346	56.90368	0.01163
5	3.396	VV	0.1067	1.17077e6	1.82958e5	91.78394
6	3.585	VB	0.0462	2.17362e5	9.24476e4	3.97791
7	3.810	BB	0.0272	890.01556	500.43295	0.06217
8	4.052	BB	0.0285	64.49979	33.59546	0.00451
9	5.012	BB	0.0352	6.30564	2.76464	0.00044
Totals :				1.43154e6	2.77398e5	

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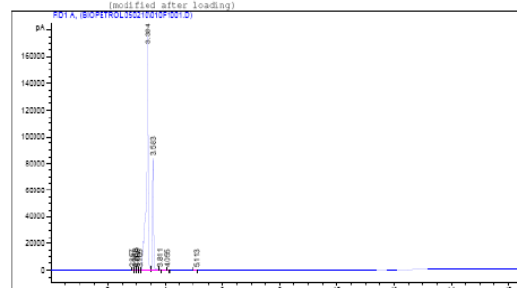
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Page 1 of 1

Sample Y1

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Sample Name: 7.2

```
=====
Acq. Operator   : F11a080210                      Seq. Line : 10
Acq. Instrument : Instrument 1                      Location : Vial 16
Injection Date  : 08/02/2010 14:57:45              Inj : 1
                                                    Inj Volume : 1 µl
Acq. Method    : C:\CHEM32\1\METHODS\1800CTANR230108.M
Last changed   : 08/02/2010 11:27:14 by F11a080210
Analysis Method : C:\CHEM32\1\METHODS\FAT1PM9.M
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Area Percent Report

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Dilution       : 1.0000
Use Multiplier & Dilution Factor with ISTDs
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Signal 1: FID1 A,

Peak #	RetTime [min]	Type	Width [min]	Area [pA*s]	Height [pA]	Area %
1	2.857	BB	0.0317	36.84271	16.82359	0.00275
2	2.938	BB	0.0302	626.24616	326.62924	0.09125
3	3.009	VV	0.0361	1474.16040	623.16537	0.11446
4	3.106	VV	0.0421	146.97446	55.87798	0.01377
5	3.394	VV	0.0983	1.03649e6	1.75647e5	91.88173
6	3.583	VB	0.0448	2.26180e5	8.40616e4	3.86806
7	3.811	BB	0.0284	770.24434	400.13443	0.06085
8	4.055	BB	0.0305	52.17012	25.88314	0.00412
9	5.113	BB	0.0457	34.25811	10.33274	0.00271
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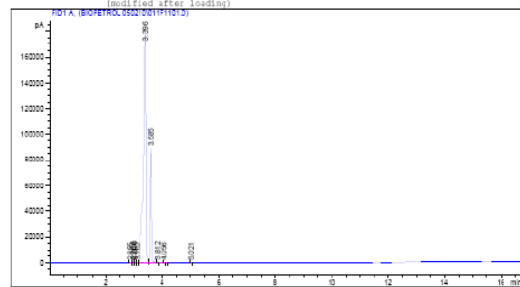
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Page 1 of 1

Sample Y2

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Sample Name: 7.3

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Acq. Operator   : F11a080210                      Seq. Line : 11
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Injection Date  : 08/02/2010 15:10:54              Inj : 1
                                                    Inj Volume : 1 µl
Acq. Method    : C:\CHEM32\1\METHODS\1800CTANR230108.M
Last changed   : 08/02/2010 11:27:14 by F11a080210
Analysis Method : C:\CHEM32\1\METHODS\FAT1PM9.M
Last changed   : 23/03/2010 14:27:59 by f11a230310
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Area Percent Report

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Dilution       : 1.0000
Use Multiplier & Dilution Factor with ISTDs
```

Signal 1: FID1 A,

Peak #	RetTime [min]	Type	Width [min]	Area [pA*s]	Height [pA]	Area %
1	2.855	BB	0.0341	37.96225	17.00202	0.00277
2	2.956	VV	0.0308	670.72114	324.56228	0.04891
3	3.006	VV	0.0382	1582.41432	628.70223	0.11539
4	3.103	VV	0.0438	146.46388	57.87811	0.01307
5	3.396	VV	0.1047	1.12175e6	1.78497e5	91.80040
6	3.585	VB	0.0461	2.46222e5	8.80876e4	3.95499
7	3.812	BB	0.0283	828.41089	434.24710	0.06041
8	4.056	BB	0.0301	63.31534	31.36975	0.00462
9	5.021	BB	0.0362	6.01198	2.53773	0.00044
Totals :				1.17733e6	2.49304e5	

*** End of Report ***

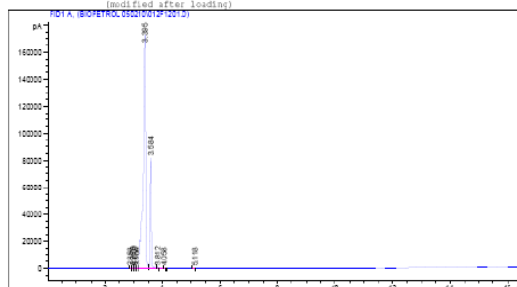
Instrument 1 23/03/2010 14:39:39 f11a230310

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Sample Y3

Data File C:\CHEM32\1\DATA\BIOFETROL 050210\012F201.D
Sample Name: 7.4

```
=====
Acq. Operator   : F11a080210                      Seq. Line : 12
Acq. Instrument : Instrument 1                      Location : Vial 12
Injection Date  : 08/02/2010 15:14:04              Inj : 1
                                                    Inj Volume : 1 µl
Acq. Method    : C:\CHEM32\1\METHODS\1800CTANR230108.M
Last changed   : 08/02/2010 11:27:14 by F11a080210
Analysis Method : C:\CHEM32\1\METHODS\FAT1PM9.M
Last changed   : 23/03/2010 14:27:59 by f11a230310
              (modified after loading)
=====
```



Area Percent Report

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Sorted By      : Signal
Multiplier     : 1.0000
Dilution       : 1.0000
Use Multiplier & Dilution Factor with ISTDs
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Signal 1: FID1 A,

Peak #	RetTime [min]	Type	Width [min]	Area [pA*s]	Height [pA]	Area %
1	2.858	BB	0.0322	37.20389	17.59138	0.00302
2	2.959	BB	0.0298	616.54887	331.55115	0.03287
3	3.010	VV	0.0361	1455.94348	607.80867	0.11823
4	3.106	VV	0.0420	116.01784	51.21688	0.01210
5	3.395	VV	0.0973	1.10805e6	1.71876e5	91.84163
6	3.584	VB	0.0448	2.20258e5	8.11008e4	3.86601
7	3.812	BB	0.0292	730.84145	391.06386	0.03935
8	4.058	BB	0.0322	53.55688	21.32040	0.00435
9	5.118	BB	0.0468	32.45870	7.64347	0.00284
Totals :				1.13314e6	2.54217e5	

*** End of Report ***

Instrument 1 23/03/2010 14:40:34 f11a230310

Page 1 of 1

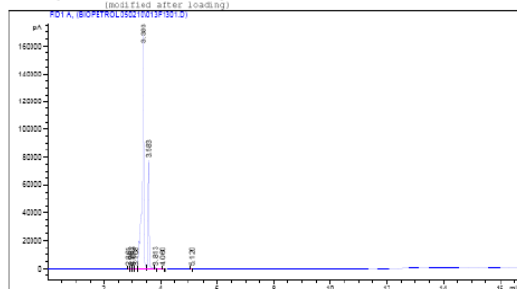
Sample Y4

Figure D.3: Sample Y

Created with

Data File C:\CHEM32\1\DATA\BIOFETROL 000210\01\F1301.D
Sample Name: 8.1

Acq. Operator : F13a080210 Seq. Line : 11
Acq. Instrument : Instrument 1 Location : Vial 13
Injection Date : 08/02/2010 16:07:22 Inj : 1
Inj Volume : 1 µl
Acq. Method : C:\CHEM32\1\METHODS\1800TAN230108.M
Last changed : 08/02/2010 11:27:14 by F13a080210
Analysis Method : C:\CHEM32\1\METHODS\FAT19AH.M
Last changed : 23/03/2010 14:27:59 by f13a230310
(modified after loadInj)



Area Percent Report

Sorted By : Signal
Multiplier : 1.0000
Dilution : 1.0000
Use Multiplier & Dilution Factor with ISTDs

Signal 1: FID1 A,

Peak #	RetTime [min]	Type	Width [min]	Area [a.u.]	Height [a.u.]	Area %
1	2.861	BB	0.3320	32.17862	15.77541	0.00291
2	2.962	BB	0.3302	581.83356	298.10976	0.05087
3	3.013	VV	0.3357	1301.40417	551.12574	0.11485
4	3.106	VV	0.3409	135.91428	51.77934	0.01190
5	3.393	VV	0.3928	9.3417965	1.6771965	91.81429
6	3.683	BB	0.3440	2.0884265	7.7637661	3.33079
7	3.813	BB	0.3290	672.66864	357.18003	0.05891
8	4.060	BB	0.3328	48.13805	22.12603	0.00422
9	5.120	BB	0.3392	25.20344	9.38992	0.00227

Totals : 1.14192e6 2.46612e5

*** End of Report ***

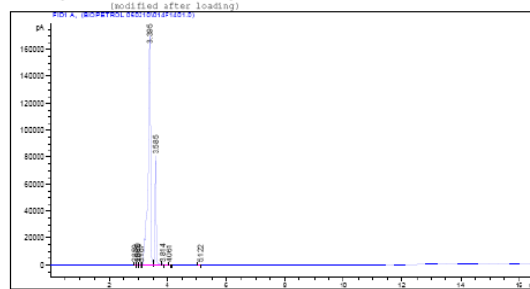
Instrument 1 23/03/2010 14:41:07 f13a230310

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Sample Z1

Data File C:\CHEM32\1\DATA\BIOFETROL 000210\01\F13403.D
Sample Name: 8.2

Acq. Operator : F13a080210 Seq. Line : 14
Acq. Instrument : Instrument 1 Location : Vial 14
Injection Date : 08/02/2010 16:30:31 Inj : 1
Inj Volume : 1 µl
Acq. Method : C:\CHEM32\1\METHODS\1800TAN230108.M
Last changed : 08/02/2010 11:27:14 by F13a080210
Analysis Method : C:\CHEM32\1\METHODS\FAT19AH.M
Last changed : 23/03/2010 14:27:59 by f13a230310
(modified after loadInj)



Area Percent Report

Sorted By : Signal
Multiplier : 1.0000
Dilution : 1.0000
Use Multiplier & Dilution Factor with ISTDs

Signal 1: FID1 A,

Peak #	RetTime [min]	Type	Width [min]	Area [a.u.]	Height [a.u.]	Area %
1	2.859	BB	0.3322	15.93518	7.53527	0.00131
2	2.960	BB	0.3302	481.38633	237.04622	0.03803
3	3.011	VV	0.3348	1127.92786	485.16526	0.09296
4	3.107	VV	0.3412	133.46275	49.36339	0.01100
5	3.395	VV	0.3949	9.00518e5	1.70351e5	95.62394
6	3.585	BB	0.3453	2.10275e5	4.09637e4	4.15404
7	3.814	BB	0.3259	717.65020	390.18511	0.06800
8	4.061	BB	0.3333	39.21896	26.78897	0.00488
9	5.122	BB	0.3444	36.94947	11.68422	0.00305

Totals : 1.21337e6 2.52504e5

*** End of Report ***

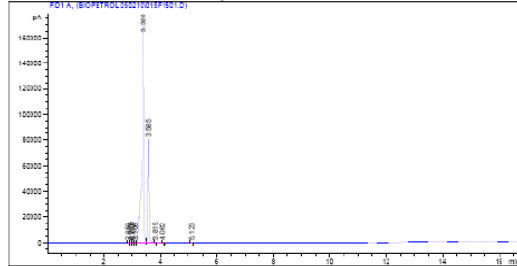
Instrument 1 23/03/2010 14:41:55 f13a230310

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Sample Z2

Data File C:\CHEM32\1\DATA\BIOFETROL 000210\01\F1301.D
Sample Name: 8.3

Acq. Operator : F13a080210 Seq. Line : 11
Acq. Instrument : Instrument 1 Location : Vial 15
Injection Date : 08/02/2010 16:53:41 Inj : 1
Inj Volume : 1 µl
Acq. Method : C:\CHEM32\1\METHODS\1800TAN230108.M
Last changed : 08/02/2010 11:27:14 by F13a080210
Analysis Method : C:\CHEM32\1\METHODS\FAT19AH.M
Last changed : 23/03/2010 14:27:59 by f13a230310
(modified after loadInj)



Area Percent Report

Sorted By : Signal
Multiplier : 1.0000
Dilution : 1.0000
Use Multiplier & Dilution Factor with ISTDs

Signal 1: FID1 A,

Peak #	RetTime [min]	Type	Width [min]	Area [a.u.]	Height [a.u.]	Area %
1	2.858	BB	0.3329	31.11638	14.16784	0.00253
2	2.959	VV	0.3304	601.50970	306.13414	0.04904
3	3.010	VV	0.3370	1380.00058	569.18392	0.11286
4	3.106	VV	0.3427	143.92206	54.15982	0.01218
5	3.396	VV	0.3985	1.05622e6	1.70215e5	91.76834
6	3.686	BB	0.3455	2.10342e5	4.11419e4	3.98871
7	3.815	BB	0.3297	712.28333	375.82609	0.05788
8	4.062	BB	0.3336	71.55166	32.12744	0.00599
9	5.123	BB	0.3415	36.30488	10.16931	0.00246

Totals : 1.23057e6 2.57270e5

*** End of Report ***

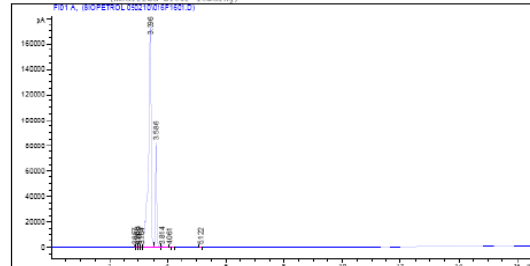
Instrument 1 23/03/2010 14:42:29 f13a230310

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Sample Z3

Data File C:\CHEM32\1\DATA\BIOFETROL 000210\01\F1301.D
Sample Name: 8.4

Acq. Operator : F13a080210 Seq. Line : 16
Acq. Instrument : Instrument 1 Location : Vial 16
Injection Date : 08/02/2010 17:16:57 Inj : 1
Inj Volume : 1 µl
Acq. Method : C:\CHEM32\1\METHODS\1800TAN230108.M
Last changed : 08/02/2010 11:27:14 by F13a080210
Analysis Method : C:\CHEM32\1\METHODS\FAT19AH.M
Last changed : 23/03/2010 14:27:59 by f13a230310
(modified after loadInj)



Area Percent Report

Sorted By : Signal
Multiplier : 1.0000
Dilution : 1.0000
Use Multiplier & Dilution Factor with ISTDs

Signal 1: FID1 A,

Peak #	RetTime [min]	Type	Width [min]	Area [a.u.]	Height [a.u.]	Area %
1	2.857	BB	0.3323	26.16569	15.55420	0.00224
2	2.958	VV	0.3305	605.60034	307.03615	0.04700
3	3.009	VV	0.3373	1434.44409	580.46148	0.11133
4	3.104	VV	0.3432	154.40757	55.21762	0.01200
5	3.396	VV	0.3913	1.04991e6	1.72770e5	91.48442
6	3.686	BB	0.3449	2.33054e5	4.27784e4	4.08754
7	3.814	BB	0.3273	3058.47407	691.08521	0.24803
8	4.061	BB	0.3321	52.31269	26.30217	0.00406
9	5.122	BB	0.3406	30.73660	10.81779	0.00239

Totals : 1.28848e6 2.57232e5

*** End of Report ***

Instrument 1 23/03/2010 14:43:13 f13a230310

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Sample Z4

Figure D.4: Sample Z

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CHAPTER 1

INTRODUCTION

1.0 Introduction

Now days, are lot of people know uses and benefits of biofuel and biofuel groups such as bioethanol, biodiesel, biogas and biopetrol has a huge potential to replace petroleum fuels in the future because there unlimited resource. Biofuel derived from plant and animals oils recently has attracted the researchers about the capabilities and renewably. Other than environmental friendly, biofuel can improve the engine vehicle efficiency and this has been proved through research that has been done. For example biodiesel, it can be performed excellent energy balance (input: 1 / Output: 2.5) which would be 78% greater than standard diesel (Herschel, 2007). Generally, biofuel is defined as a liquid or gaseous fuel that can be produced from the utilization of biomass substrates according to Giampietro et al. (Tamunaidu and Bhatia, 2006). In this research, production of biopetrol by using fatty acid as the raw material is the main topic that being focused.

Commonly, natural triglycerides present in vegetable oil are extracted into several oil components using transterification route but it generates a large amount of glycerin (byproduct) thus difficult to purify. Therefore, heterogeneous catalytic cracking method is suggested. However, triglyceride molecules are too large to enter the pores of Zeolite (Dupain *et al*, 2006) during heterogeneous catalytic cracking; therefore this research is proceeding within vegetable oil derived or fatty acid into biopetrol at 1 atm and at 98 °C. In this case, oleic acid ($C_{18}H_{34}O_2$) has been chosen for conversion into

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isooctane which also the major constituents of biopetrol since that oleic acid contain low in sulfur and nitrogen besides it also encounter more than 40% constituents inside most of the vegetable oil such as palm oil, olive oil, rapeseed and others. Beside, Zeolite also is chosen because it possesses a catalytic activity that is much higher than other types of catalysts because of its high selectivity properties.

Twaiq *et al* in his paper claimed that, recently several researchers have been successful in production of hydrocarbons from palm oil mainly bio-gasoline or biopetrol (Tamunaidu and Bhatia, 2006) which have been carried out using cracking catalysts in a micro-reactor but still not valid for commercialize. It also has generated a significant of interest of Palm Oil Research Institute of Malaysia (PORIM) in development of biodiesel from palm oil. (Hussain *et al*, 2006).

1.1 Problem Statement

Currently, the world is depending to the only major source of energy as known as the petroleum fossil fuel. It is a nonrenewable energy and the next few decades the source to the crude oil will be finished. The idea of this research is to solve out the fuel crises that really need to have other alternative.

As we know, now day the amounts of petroleum fossil reserve in this world are decreasing and this problem also includes Malaysia such as the saying of Prime Minister Datuk Seri Najib Razak *“Malaysia is an oil exporter, but if we do not find new oil reserves, then by 2009, we will become a net importer”*. Since then, the prices of fuel are increasing gradually every year. Figure 1.1 is the fuel price in Malaysia from May 2004 to June 2008 and as we can see the fuel price increase from RM 1.37 per Liter to RM 2.70 per Liter in this four year. After June 2008, the fuel price starts to decrease slowly until RM 1.80 per Liter 2009 for RON95 and it maintain until now. Figure 1.2 shows the decreasing fuel price after June 2008. This price is still the highest compared to the price in May 2004.



Figure 1.1 : Fuel Price in Malaysia from May 2004 to June 2008

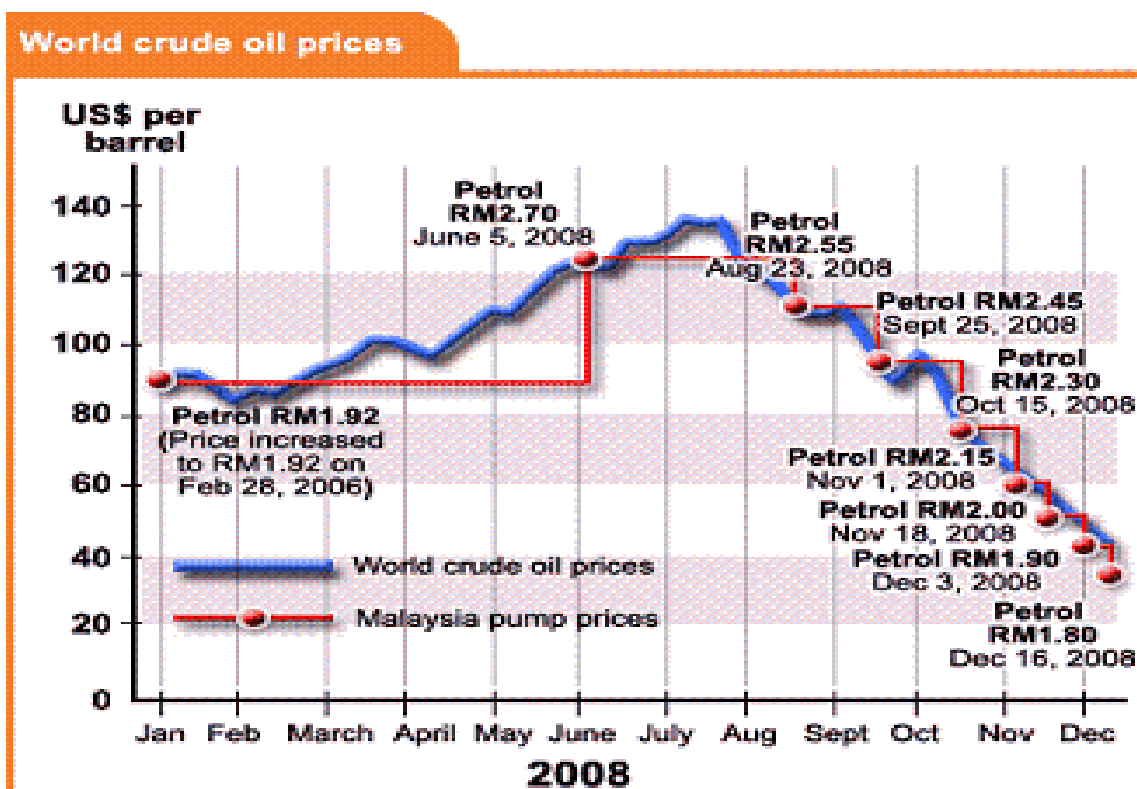


Figure 1.2 : World Crude Oil & Malaysia fuel Prices from Jan to Dec 2008.

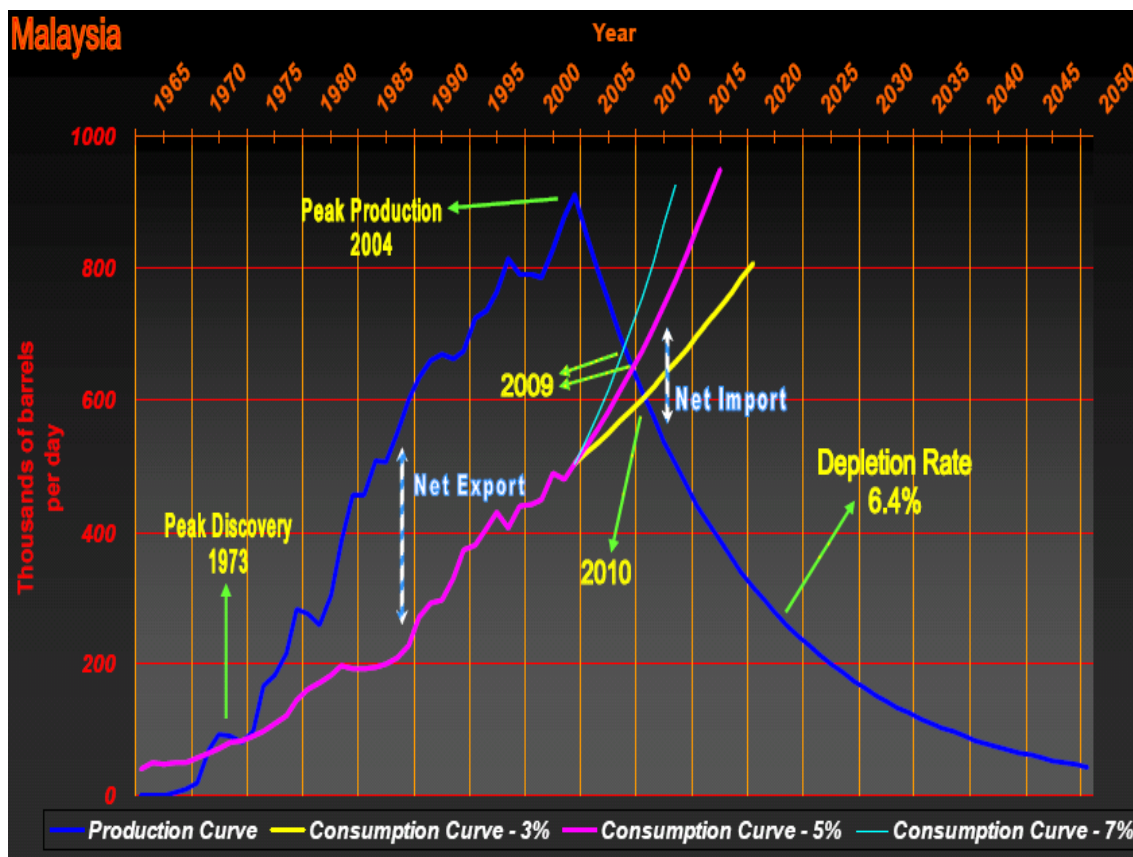


Figure 1.3 : Malaysia's Looming Energy Crisis (M. Noor, 2008)

Malaysia is one of the major oil exporters in the world. Malaysia also has the crisis of the declining of these mineral sources. Malaysia's oil production is decreasing in 2004 and would then decline by 6.4 percent annually. Figure 1.1 shows the declining Malaysia oil's production by 2004. Forecast, by 2009 to 2010 Malaysia will become a net importer because out of mineral sources (petroleum) and the demand of oil increasing. From figure 1.4, the blue line represents the production of oil which is 820,000 barrels per day in 1998 and decreasing to 620,000 barrels per day in 2008. Within 10 years from now, all of crude oils will finish up without any preservation awareness. Figure 1.2 shows the fuel price in Malaysia from May 2004 to Jun 2008. Bio-petrol is one of bio-fuels which can be fuel alternatives in substituting petrols and diesel.

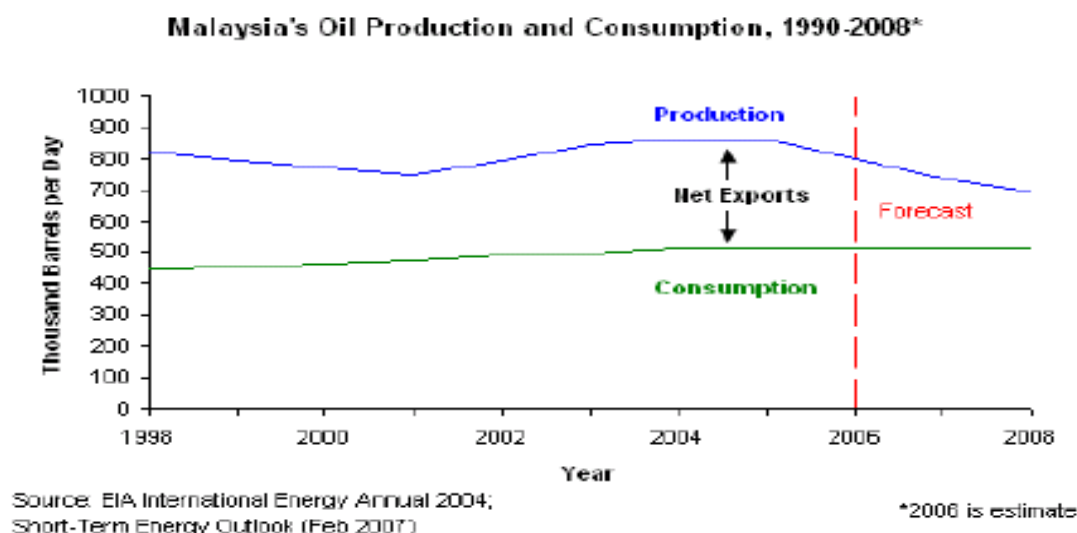


Figure 1.4: Malaysia's Oil Production and Consumption

Now, a few plants are using biomass energy technologies use waste or plant matter to produce energy with a lower level of greenhouse gas emissions than fossil fuel sources. Most of countries aware of this issue and they tend to develop research and modern technology to produce biofuels.

At an average, about 0.1 tonne of Palm Oil Mill Effluent (POME) is generated for every tone of fresh fruit bunch processed. POME consists of water soluble components of palm fruits, saturated fatty acids as oleic acid, stearic acid and palmitic acid and also suspended materials as palm fiber and oil. Despite of its biodegradability, the POME cannot be discharged without treating it. This is because POME is very acidity and could pollute environment. By thinking of this, producing biopetrol from the POME can be the alternative solutions for treating the POME. At the same time, contribute to the production of biopetrol from the fatty acids.

Oleic acid is the dominative component in palm oil waste. Its disposal into water supply sources causes serious water pollution. Besides that the loss of oleic acid as a useful industrial component also occurs so that it is not utilized much and always eliminated to improve and upgrade the quality of crude palm oil. Thus, it is disposed as palm oil waste and then pollutes water resources by its spillage. Producing petrol from the waste of palm oil will give an alternative choice to the users, especially for petrol-

engine vehicles' owners. In addition, this biopetrol, which is graded 100 for its octane number, burns very smoothly so biopetrol can reduce emissions of some pollutants (Omar, 2005).

According to the previous research, the yield of biopetrol using thermal cracking is very small. In this research, the concentration of isooctane that is produced from oleic acid and also the conversion of fatty acids to form desired isooctane in biopetrol will be improved by using heterogeneous catalytic cracking process and use zeolite as catalyst.

1.2 Objectives

- I. To analyze isooctane obtained from oleic acid ($C_{18}H_{34}O_2$).
- II. To find and determine concentration of synthesized biopetrol obtained.
- III. To improve the concentration of biopetrol (isooctane) obtained from oleic acid using zeolite as catalyst through-Heterogeneous catalysis.

1.3 Scopes of Study

In order to accomplish the objectives, the scope of this research is focusing on the criteria that are stated as below:-

- I. Application of the heterogeneous catalytic cracking process to crack the long-chain oleic acid molecules into the smaller hydrocarbon molecules instead of previous thermal cracking.
- II. Identification of the composition of isooctane using Gas Chromatography method.
- III. Determination of the amount of isooctane through analysis using Gas Chromatography method.

- IV. Description of the molecular arrangement during isomerization of oleic acid through catalytic cracking process with the presence of catalyst.
- V. Comparison of isooctane obtained and the mode of catalysis process with previous research.

1.4 Rational and Signification

- I. Biopetrol is biodegradable and renewable resource, able to sustain the energy supply for transportation.
- II. Oleic acid can be found easily in most vegetable oil especially in palm oil (Malaysia) and wider the palm oil application for biopetrol.
- III. The rate of plant growth is much faster than the formation of petroleum oil thus plant has widely potential as sustainable energy.
- IV. Isooctane (B100) obtain in biopetrol by catalytic cracking reduce the hydrocarbon chain cause effective combustion in petrol engine and increase engine life.
- V. Biopetrol is sulphur free and able to reduce the emission of green emission gas more than 40 percent.
- VI. Catalytic cracking provide higher conversion of hydrocarbon than thermal cracking does by lowering the activation energy of the reaction.